Commonwealth of Kentucky Division for Air Quality

PERMIT APPLICATION SUMMARY FORM

Completed by: Andrew True

| GEN | NERAL INFORMATION: | | |
|------|---|---------------------------------------|--------------------|
| | Name: | Buffalo Creek Energy, LLC | 7. |
| | Address: | Adjacent to Kentucky 460, 41603/41501 | Tram/Pikeville, KY |
| | Date application received: | 4/21/2011 | |
| | SIC Code/SIC description: | 2999, Products of Petroleur | m and Coal, NEC |
| | Source ID: | 21-195-00287 | ii una coui, i de |
| | Agency Interest: | 111332 | |
| | Activity: | APE20110001 | |
| | Permit: | F-11-031 | |
| Д рр | PLICATION TYPE/PERMIT ACTIVE | ITV• | |
| | [X] Initial issuance | [] General permit | |
| | [] Permit modification | [X] Conditional major | |
| | Administrative | [] Title V | |
| | Minor | [X] Synthetic minor | |
| | Ninor Significant | [] Operating | |
| | [] Permit renewal | [X] Construction/operating | |
| Cor | MPLIANCE SUMMARY: | | |
| CON | | [] Compliance sch | adula inaludad |
| | [] Source is out of compliance [X] Compliance certification signed | [] Compliance sch | edule included |
| APP | PLICABLE REQUIREMENTS LIST: | | |
| | [] NSR | [X] NSPS | [X] SIP |
| | Non-Attainment | [] NESHAPS | [] Other |
| | PSD | [] CAM | |
| | Netted out of PSD/NSR | | |
| | Not major modification p | per 401 KAR 51:001, 1(116)(| b) |
| Mis | SCELLANEOUS: | | |
| | [] Acid rain source | | |
| | Source subject to 112(r) | | |
| | [X] Source applied for federally en | forceable emissions cap | |
| | [] Source provided terms for altern | <u>-</u> | |
| | [X] Source subject to a MACT stan | | |
| | [] Source requested case-by-case | | |
| | [] Application proposes new contr | = = = | |
| | [X] Certified by responsible officia | | |
| | [X] Diagrams or drawings included | | |
| | [] Confidential business information | | ation |
| | [] Pollution Prevention Measures | . , , 11 | |
| | [] Area is non-attainment (list poll | lutants): | |
| | • | | |

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EMISSIONS SUMMARY:

| Pollutant | Potential | |
|------------------------|--------------|--|
| | (tpy) | |
| PM | 63.51 | |
| PM ₁₀ | 55.27 | |
| PM _{2.5} | 49.62 | |
| NO _x | 48.73 | |
| SO ₂ | 92.07 | |
| СО | 66.08 | |
| VOC | 51.50 | |
| H_2S | 1.11 | |
| LEAD | 0 | |
| Single HAPs: | | |
| methanol | 2.97 | |
| benzene | 0.03 | |
| isooctane | 0.01 | |
| toluene | 0.04 | |
| ethylbenzene | 0.02 | |
| xylene | 0.02 | |
| isopropyl benzene | 0.01 | |
| 1,2,4 trimethylbenzene | 0.01 | |
| cyclohexane | 0.01 | |
| hexane | 0.02 | |
| COS | 0.30 | |
| Ni(CO)4 | 0.04 | |
| HCN | 0.07 | |
| HCl | 0.07 | |
| HG | 0.10 | |
| Source wide HAPs | 3.71 | |
| GHG Emissions: | | |
| CO ₂ | 3,946,558.18 | |
| CH ₄ | 6.39 | |
| CO ₂ e | 3,946,692.29 | |

SOURCE DESCRIPTION:

On April 21, 2011, the source applied to the Division for the construction/operation of a Petroleum and Coal Products Manufacturing facility adjacent to KY-460 near Tram/Pikeville, Kentucky 41603/41501. The facility will produce gasoline and liquefied petroleum gas (LPG) from coal as

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well as elemental sulfur. The facility will utilize multiple processes. Coal will be used as a raw material fed to a gasification process to produce syngas. The syngas will then undergo a cleaning process where impurities (major impurities are sulfur and mercury), will be removed. The cleaned syngas will then be modified to produce methanol. The methanol will then be fed to a methanol to gasoline (MTG) process to produce gasoline.

Some of the facility's processes will produce steam which will be used to provide process heat as needed, feed steam driven sections of the process, or will be converted into electrical power as needed to drive electrical systems. A cooling tower will allow process water to be cooled and reentered into the process. Electric power produced by the process steam will be utilized at the facility and additional needs for electric will be supplied by utility connections. There will be no sales of electric power.

The maximum coal input will be 346 tons per hour (3,030,960 tons per year) into the systems and produce 18,000 barrels (42 gallons/barrel) of gasoline per day and 6,570,000 barrels per year. Raw materials for the plant will be trucked into the site. Product gasoline and LPG will be removed from the site via the preferred method of loading to railcar and some allowance is made for trucking for the delivery to markets.

The facility is divided into several areas for the purpose of permitting:

(1) Material Handling, Storage Sizing, & Preparation

- Handling, preparation, and storage of coal, limestone, ash/slag, and filter cake.
- Paved haul roads

(2) Gasification & Gas Cleanup

- Mill Heaters, Startup vessels, lock hoppers, CO₂ Purification Unit,
- Acid Gas Removal (removes the acid gases CO₂, H₂S, COS, mercury, and HCN)

(3) MTG (Methanol to Gasoline Plant)

- MTG Fired Heaters
- -MTG Regeneration Off-Gas
- -Methanol to Gasoline Plant Flared stream

(4) Other Equipment/Emission Units

- -Flare
- -Cooling Tower
- -Methanol Tank
- -Gasoline Storage Tanks
- -Sulfur (liquid) Storage Tank
- -Sulfur Vehicle Loading
- -Gasoline Loading Racks
- LPG Loading Racks
- -Start-up Boiler/Process Heater
- -MTG Regeneration Off-Gas
- -Methanol to Gasoline Plant Flared stream
- -Fugitive Equipment Leaks

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EMISSIONS AND OPERATING CAPS DESCRIPTIONS:

Source Wide Emission Limitations:

To preclude the applicability of 401 KAR 52:020, *Title V permits*, and 401 KAR 51:017, *Prevention of significant deterioration of air quality*, the source wide emissions shall not equal or exceed the following limits on a consecutive twelve (12)-month basis:

- (1) $PM_{10}/PM_{2.5}$ emission of 90 tons per year;
- (2) NO_X emission of 90 tons per year;
- (3) SO_2 emission of 94 tons per year;
- (4) CO emission of 90 tons per year;
- (5) VOC emission of 90 tons per year;
- (6) COS emissions of 9.0 tons per year;
- (7) CH_3OH emissions of 9.0 tons per year;
- (8) Single HAPS of 9.0 tons per year; and
- (9) Combined HAP emission of 22.5 tons per year.

The Division evaluated the sources potential to emit and determined that the source's potential emissions do not exceed the emission limits described above. Physical and/or operational limitations on the capacity of the source to emit PM₁₀/PM_{2.5}, NO_X, SO₂, CO, VOC, COS, CH₃OH, and HAPS that are enforceable as a practical matter are contained in Section B of the permit. The source-wide emission limitations for PM₁₀, PM_{2.5}, NO_X, CO, VOC, COS, CH₃OH, SO₂, and HAPS specified in Section D of the permit are set below the major source thresholds for each pollutant.

The following are emission units in Section B of the permit:

| Emission Unit/Point ID | Description |
|------------------------|---|
| TPC1-12 | Coal Transfer Points and Conveyors |
| CR1 | Coal Crusher |
| PR | Paved Haulroads |
| FH 1, 3, 5, 7, 9 | Coal Feed Bunkers |
| TPA1-5 | Ash/Slag Transfer Points and Conveyors |
| SSP | Ash/Slag Stockpile |
| В | Load-out Bin |
| TPFC 1&2 | Filter Cake Transfer Points and Conveyors |
| FCS1 | Filter Cake Silo |
| TPL1-5 | Transfer Points and Conveyors |
| CR7 | Limestone Crusher |
| LS | Limestone Stockpile |
| FH 2, 4, 6 8, 10 | Limestone Feed Bunkers |
| A1/1 - A1/5 | Mill and Heaters |
| A2/1 | Startup Vessel No.1 |
| A2/2 | Startup Vessel No.2 |
| B1/1 | Lock Hoppers No.1-6 (Feed Bunker No.1) |
| B1/2 | Lock Hoppers No.7-12 (Feed Bunker No.2) |
| C1 | CO ₂ Purification Unit |

| C2 | Acid Gas (CO ₂ /H ₂ S) Removal | |
|--------------|--|--|
| E1 (SUDCH) | MTG Fired Heater | |
| E1 (SURGH) | (Start-Up/Regeneration Gas Heater) | |
| E2 (CLIDII) | MTG Fired Heater | |
| E2 (SURH) | (Start-Up/Reactivation Heater) | |
| E2 (DCH) | MTG Fired Heater | |
| E3 (RCH) | (HGT Reactor Charge Heater) | |
| E4 | MTG Regeneration Off-Gas | |
| E5 | Methanol to Gasoline Plant | |
| E5 | Flared Process Stream from MTG | |
| FL | Flare | |
| B2/1 (FL ST) | Gasifier Startup (flared streams) | |
| B2/2 (FL ST) | Gasifier Startup (flared streams) | |
| G | Pilots on Flare | |
| CT | Cooling Tower | |
| TK6 | Methanol Tank | |
| TK1 | Gasoline Storage Tank No.1 | |
| TK2 | Gasoline Storage Tank No.2 | |
| TK3 | Gasoline Storage Tank No.3 | |
| TK7 | Sulfur (liquid) Storage Tank | |
| SVL | Sulfur Vehicle Loading | |
| LR1 | Loading Rack No.1 | |
| LR2 | Loading Rack No.2 | |
| LPGL | LPG Loading | |
| F (SUSB) | Startup Boiler – Process Heater | |
| FUGL | Fugitive Equipment Leaks | |
| GFUG | Gasoline System Fugitives | |
| MFUG | Methanol System Fugitives | |

Emission Limitations:

| Emission Unit or Emission Point ID | Emission limit | Pollutant(s) limited |
|---|--|--|
| (BC1-6) TPC1-12, CR1, CS, FH 1, FH3, FH5, FH7, FH9 | < 10 percent opacity | Opacity |
| (BC1-6) TPC1-12, CR1, CS, FH 1, FH3, FH5, FH7, FH9 | < 0.023 g/dscm (0.010 gr/dscf) | PM/PM ₁₀ /PM _{2.5} |
| FH1-FH10, CR1, CS, SSP, | $E_{Allowable}$ =2.34 lb/hr for P less than or equal to 0.5 ton/hr =3.59 * $P^{0.62}$ for P greater than 0.5 | PM |

| FCS1, CR7, LS | ton/hr but less than or equal to 30 ton/hr =17.31 * P ^{0.16} for P greater than 30 ton/hr | |
|--|---|---|
| | [401 KAR 59:010 Section 3(2)] | |
| (BC1-6) TPC1-12, CS, PR, TPA 1-5, SSP, TPFC 1 & 2, FCS1, TPL 1-5 | Visible fugitive dust emissions beyond the property line is prohibited. [401 KAR 63:010] | PM/PM ₁₀ /PM _{2.5} |
| CR7, LS, FH 2, FH4, FH6, FH8, FH10 | Table 2 of 40 CFR 60 Subpart OOO (stacks) | PM/PM ₁₀ /PM _{2.5} |
| TPL 1-5 | Table 3 of 40 CFR 60 Subpart OOO (Fugitives) | PM/PM ₁₀ /PM _{2.5} , Opacity |
| A1/1 – A1/5, A2/1, A2/2, B1/1, B1/2 | E _{Allowable} =2.34 lb/hr for P less than or equal to 0.5 ton/hr =3.59 * P ^{0.62} for P greater than 0.5 ton/hr but less than or equal to 30 ton/hr =17.31 * P ^{0.16} for P greater than 30 ton/hr | PM/PM ₁₀ /PM _{2.5} |
| | [401 K/IK 37.010 Section 3(2)] | |
| A1/1 – A1/5, A2/1, A2/2, B1/1, B1/2 | <20 % Opacity, [401 KAR 59:010 Section 3(1)(a)] | Opacity |
| A1/1 – A1/5, A2/1, A2/2, B1/1, B1/2 | 40 CFR 60 Subpart Y limits | PM/PM ₁₀ /PM _{2.5} , Opacity |
| C1, C2 | H ₂ S < ten (10) gr/100 dscf (165 ppm by volume) at zero (0) percent O ₂ or without reducing the concentration by 85 percent, based on a three (3) hour average. [401 | H ₂ S |

| | KAR 59:105] | |
|---|---|--|
| C1, E1 (SURGH), E2 (SURH), E3 (RCH), E4, E5, FL, G, B2/1 (FL ST), B2/2 (FL ST), E5 (FL), TK7, SVL, (GFUG), (MFUG), and (FUGL) | < Quantities or duration as to be harmful to the health and welfare of humans, animals and plants. [401KAR 63:020] | hazardous matter or toxic substances |
| E1 | No gases that contain SO_2 in excess of 50 percent (0.50) of the potential SO_2 emission rate and no gases containing SO_2 in excess of 260 ng/J (0.60 lb/MMBtu) heat input. | SO_2 |
| E1 | <20 percent opacity [40 CFR 60.43c (c)] | Opacity |
| E1 | No gases that contain PM >13 ng/J (0.030 lb/MMBtu) heat input | PM |
| E2 (SURH) | No gases that contain SO ₂ in excess of 87 ng/J (0.20 lb/MMBtu) heat input or 8 percent (0.08) of the potential SO ₂ emission rate (92 percent reduction) and 520 ng/J (1.2 lb/MMBtu) heat input. [40 CFR 60.42b (k)(1)] SO ₂ emissions shall not exceed 0.819 lb/MMBtu [401 KAR 59:015, Section 5 (1) (c)] | SO_2 |
| E2 (SURH) | No gases that contain NO _X (expressed as NO ₂) in excess of 210 ng/J (0.50 lb/MMBtu) heat input | NO _x |

| E2 (SURH) | No gases any gases that contain PM in excess of 13 ng/J (0.030 lb/MMBtu) heat input. | PM |
|---------------|---|--------------------------|
| E2 (SURH) | <20 percent opacity | Opacity |
| E3 (RCH) | < 0.266 lb/MMBTU. | PM |
| E3 (RCH) | < 20% Opacity | Opacity |
| E3 (RCH) | <0.819 lb/MMBTU | SO_2 |
| FL | No gases from the flare that contain H ₂ S that exceed ten (10) gr/100 dscf (165 ppm by volume) at zero (0) percent O ₂ or without reducing the concentration by 85 percent, based on a three (3) hour average. | $ m H_2S$ |
| FL | 20 percent for more than three (3) minutes in any one (1) day | Opacity |
| СТ | No visible fugitive dust emissions beyond the lot line of the property | PM |
| TK1, TK2, TK3 | 40 CFR 63.423 requirements | VOC/HAP |
| TK7, SVL | No gases that contain H ₂ S that exceed ten (10) gr/100 dscf (165 ppm by volume) at zero (0) percent O ₂ or without reducing the concentration by 85 percent, based on a three (3) hour average. | $\mathrm{H}_2\mathrm{S}$ |

| LR1, LR2, LPGL | Emissions to the atmosphere from the vapor collection system due to the loading of liquid product into gasoline tank trucks are not to exceed 35 milligrams of total organic compounds per liter of gasoline loaded. | VOC |
|----------------|--|-----------------|
| LR1, LR2 | 40 CFR 63.422 limitations | VOC |
| F (SUSB) | < 0.266 lb/MMBTU | PM |
| F (SUSB) | < 20 percent | Opacity |
| F (SUSB) | < 0.819 lb/MMBTU. | SO_2 |

Operating Limitations:

| Emission Unit or Emission | O | D-11-44(-) 1::41 |
|--|--|---|
| Point ID | Operating limit | Pollutant(s) limited |
| (TPC1-12, TPA1-5, TPFC1-2), CR7 | Install and Operate with specified enclosures | PM/PM ₁₀ /PM _{2.5,} Opacity |
| CR1 | Install and Operate with specified Baghouse | PM/PM ₁₀ /PM _{2.5,} Opacity |
| CS | Coal Stockpiles enclosed in building(s) vented to Baghouse(s) | PM/PM ₁₀ /PM _{2.5} , Opacity |
| PR | Watering Trucks/Wet Dust Suppression consistent with good air pollution control practices for minimizing emissions | PM/PM ₁₀ /PM _{2.5,} Opacity |
| FH1-10 | Install and operate vent filter | PM/PM ₁₀ /PM _{2.5} , Opacity |
| Transfer Points and Conveyors (TPC1-12) | 3,030,960 tons/year per transfer point/conveyor | PM/PM ₁₀ /PM _{2.5} |
| CR1 | 346 tons/hour (tph) | PM/PM ₁₀ /PM _{2.5} |
| TPA1-5 | 604,440 tons per year each transfer point/conveyor | PM/PM ₁₀ /PM _{2.5} |
| TPFC1 & TPFC2 | 61,320 tons/year each | PM/PM ₁₀ /PM _{2.5} |
| LS | Limestone Stockpiles enclosed in building(s) vented to Baghouse(s) | PM/PM ₁₀ /PM _{2.5} PM/PM ₁₀ /PM _{2.5} |
| Material Handling, Storage Sizing, & Preparation | reasonable precautions shall be taken to prevent particulate | PM/PM ₁₀ /PM _{2.5} , Opacity |

| (all units subject to 401 KAR 63:010) | matter from becoming airborne | |
|---------------------------------------|--|--|
| TPL 1-5 | 166,440 tons/year each (feed rate to plant), 100 tph bin filling rate | PM/PM ₁₀ /PM _{2.5} , Opacity |
| CR7 | 166,440 tons/year each (feed rate to plant) 100 tph bin filling rate | PM/PM ₁₀ /PM _{2.5} , Opacity |
| LS | 0.2 mmscf/hr vented through baghouse | PM/PM ₁₀ /PM _{2.5} , Opacity |
| A1/1 – A1/5 | 3,030,960 tons per year coal for gasification | NO _x , CO, VOC, PM, PM _{2.5} , PM ₁₀ |
| A1/1 – A1/5 | During Normal Plant Operation, the permittee shall not operate more than four (4) units, two (2) units per gasifier, when the full plant is operational. | NO_x , CO, VOC, PM, $PM_{2.5}$, PM_{10} |
| | (One (1) unit must be in standby and NOT operating when the full plant is operational.) | |
| A1/1 – A1/5 | During cold startup, the permittee shall use only one unit with natural gas when hydrogen is not available for fuel and the remaining units shall be started on hydrogen. The duration of cold startups per year shall be limited to 40 (forty) hours. | NO _x , CO, VOC, PM, PM _{2.5} , PM ₁₀ |
| | Any one (1) unit may be used for coal startup. | |
| A2/1 | 15,570 tons per year coal for gasification and 173 tons/hr. 31.5 million standard cubic feet (mmscf) gas discharge per /year 90 hours of startup/year | SO ₂ , CO, VOC, PM, PM _{2.5} , PM ₁₀ |
| A2/2 | 15,570 tons per year coal for gasification and 173 tons/hr. 31.5 million standard cubic feet (mmscf) gas discharge per /year | SO ₂ , CO, VOC, PM, PM _{2.5} , PM ₁₀ |

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| | 90 hours of startup/year | |
|-------------------------------------|--|---|
| B1/1 | 1,515,480 tons per year coal for gasification and 173 tons/hr | |
| | 7008 mmscf discharge from lockhopper/year and an additional 0.57 mmscf/hr allowed during 30 feedstock changes per year | SO ₂ , CO, VOC, PM, PM _{2.5} , PM ₁₀ |
| B1/2 | 1,515,480 tons per year coal for gasification and 173 tons/hr | |
| | 7008 mmscf discharge from lockhopper/year and an additional 0.57 mmscf/hr allowed during 30 feedstock changes per year | SO ₂ , CO, VOC, PM, PM _{2.5} , PM ₁₀ |
| Gasification and Cleanup Units | The permittee shall use PRB-coal or other low sulfur coal with a maximum sulfur content of 0.5% during startup. | SO_2 |
| Gasification and Cleanup Units | When reasonably possible, low sulfur coal shall be reintroduced for shutdowns. | SO_2 |
| C1 | Install and operate CO ₂ Stripping and/or Catalytic Purification unit | CO, H ₂ S and VOC |
| C1 | Regeneration off-gas rate from the MTG plant (regeneration of catalyst) shall not exceed 356.3 MMscf per year. | CO, SO ₂ |
| C1 | The mass flow rate of off-gas from the AGR system shall not exceed 3,058,660 tons per year. | CO, SO ₂ |
| C1 | 8,000 hours per year of operation | CO, SO_2 |
| C2 | 280 metric tons of gas flared per year | NO _x , SO ₂ , CO, VOC, HAPS |
| E1 (SURGH) E2 (SURH) E3 (RCH) | Combustion of syngas fuel only, except for 40 hours per year when the MTG tailgas (secondary fuel) is utilized (exception is for E3 only). | NO _x , SO ₂ , CO, VOC, PM, PM _{2.5} , PM ₁₀ |
| E5 | 31,120 pounds per year flared | NO _x , CO, VOC |
| FL | Gas production sent to the flare shall be limited to | NO_x , SO_2 , CO , VOC , PM , $PM_{2.5}$, PM_{10} |

| | 100,000 m ³ n/event (start-up + | |
|--------------------|--|---|
| FL | shutdown) per gasifier. Gas production sent to the flare shall be limited to 6,000,000 | NO _x , SO ₂ , CO, VOC, PM, |
| | m ³ n/year (start-up + shutdown) from the gasifiers. Comply with 40 CFR 60.18 | PM _{2.5} , PM ₁₀ NO _x , SO ₂ , CO, VOC, PM, |
| FL | - 1 | PM _{2.5} , PM ₁₀ |
| FL | Flare shall be equipped with a wind deflector designed to stabilize the flare flame, positively influencing the flame and efficiency of combustion and pollution control efficiency of regulated air pollutants. | NO _x , SO ₂ , CO, VOC, PM, PM _{2.5} , PM ₁₀ |
| FL | The permittee shall use, whenever the flare is in operation, natural gas fuel | NO _x , SO ₂ , CO, VOC, PM, PM _{2.5} , PM ₁₀ |
| СТ | Maintain the total dissolved solids (TDS) concentration in the circulation cooling water at or below 5,000 ppm. | PM, PM _{2.5} , PM ₁₀ |
| СТ | The cooling tower shall not be operated with chromium-based water treatment chemicals | To preclude applicability of 401 CFR 63 Subpart Q |
| СТ | Reasonable precautions to prevent particulate matter from becoming airborne. | PM, PM _{2.5} , PM ₁₀ |
| TK1, TK2, TK3, TK6 | Fixed roof in combination with an internal floating roof meeting | VOC, HAPs |
| TK1, TK2, TK3 | Most Stringent between: 40 CFR 60 Subpart Kb or 40 CFR 63 Subpart R | VOC, HAPs |
| SVL | Maximum sulfur vehicle loading shall not exceed 51.6 million pounds (lb) per year. | H_2S |
| TK7 | Degassing and/or sweep air from the sulfur storage tank shall be incinerated in the SRU furnace or vented to the flare. | H_2S |
| SVL | The sulfur loading rack shall be equipped with a vapor recovery system and the unit shall be vented to the flare. | H_2S |

| LPGL | 40 CFR 60 Subpart XX | VOC |
|------------------|---|--|
| LR1 and LR2 | 40 CFR 60 Subpart XX and 40 CFR 63 Subpart R restrictions | VOC |
| F(SUSB) | Combust natural gas or LPG only | CO , NO_X , SO_2 , and $PM/PM_{10}/PM_{2.5}$ |
| F(SUSB) | Maximum operation at full capacity (81.84 mmBtu/hr) shall be limited to 384 hours per year based on a twelve (12) month rolling total. | CO, NO _X , SO ₂ , and PM/PM ₁₀ /PM _{2.5} , VOC |
| FUGL, MFUG, GFUG | Implement a Leak Detection and Repair (LDAR program) | VOC/HAPs |
| FUGL, MFUG, GFUG | All valves, compressors, open ended lines, and sampling connections for which a control efficiency of 99% has been applied shall have the following modifications/design: (1) Valves must be designed to be sealless; (2) Compressors shall have dual mechanical seal with barrier fluid maintained at a higher pressure than the compressed gas; (3) Open ended lines must have a properly installed blind, cap, plug, or second valve on the open end; (4) Sampling connections, a closed-loop sampling system must be used. (5) Pumps must have a sealless design or dual mechanical seal with barrier fluid maintained at a higher pressure than the pumped fluid. | VOC/HAPs |
| FUGL, MFUG, GFUG | All connectors for which a control efficiency of 100% has been applied shall be properly welded to eliminate emissions. | VOC/HAPs |
| | All compressors for which a control efficiency of 90% has been applied shall utilize a | |

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| closed vent system routed to a | |
|--------------------------------|--|
| control device. | |

OPERATIONAL FLEXIBILITY:

None